

Influence du confinement sur différents régimes d'ébullitions

A. della Volpe, [N. Baudin](#), S. Roux, R. Yu, J-M. Fiard, J. Bellettre

Summary

- 01** Introduction & context
- 02** Experimental apparatus
- 03** Results & Data analysis
- 04** Conclusion & perspectives

Introduction & context

Interest of immersion cooling for automotive field

EVs components thermal outputs steadily increasing:

- Controllers/processors
- Battery thermal management & A/C
- Powertrain

Pool boiling: simple system, passive (no pump required)

Need to enhance efficiency and compactness ->

confined boiling

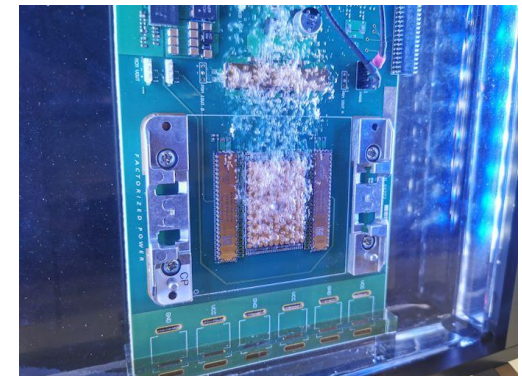
Confinement -> **risk of critical heat flux**



Need for specific study with a dielectric fluid
Construction of new test bench



Today: 130kW DC charge
Target: 350kW DC charge



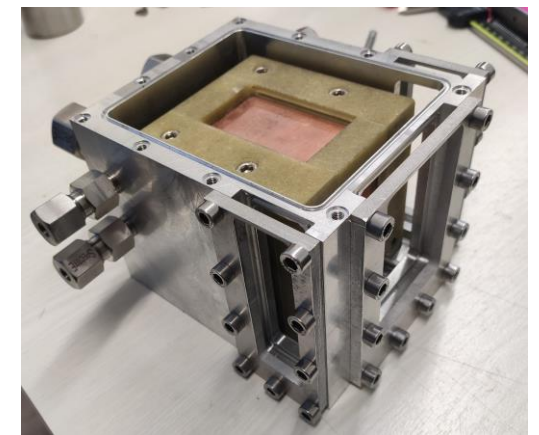
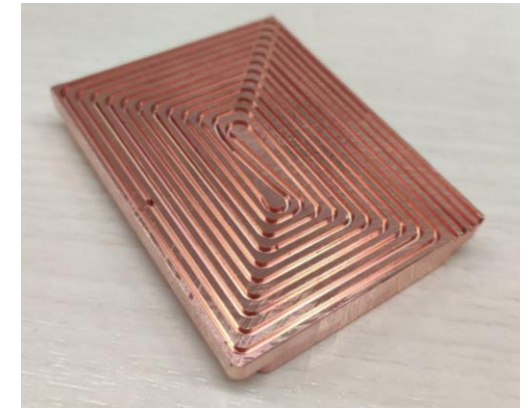
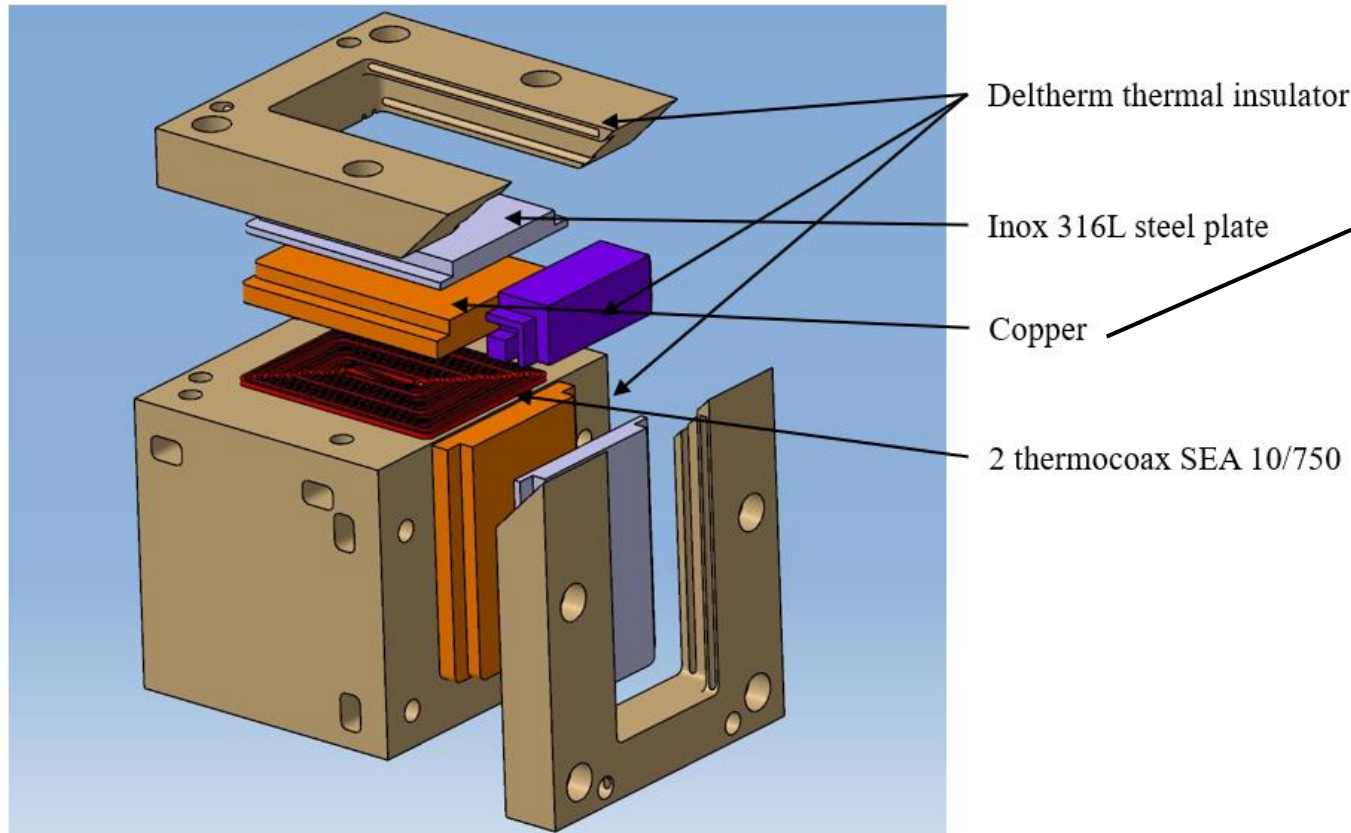
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Experimental apparatus

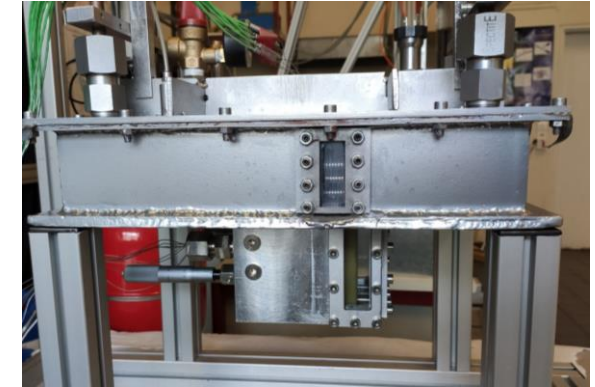
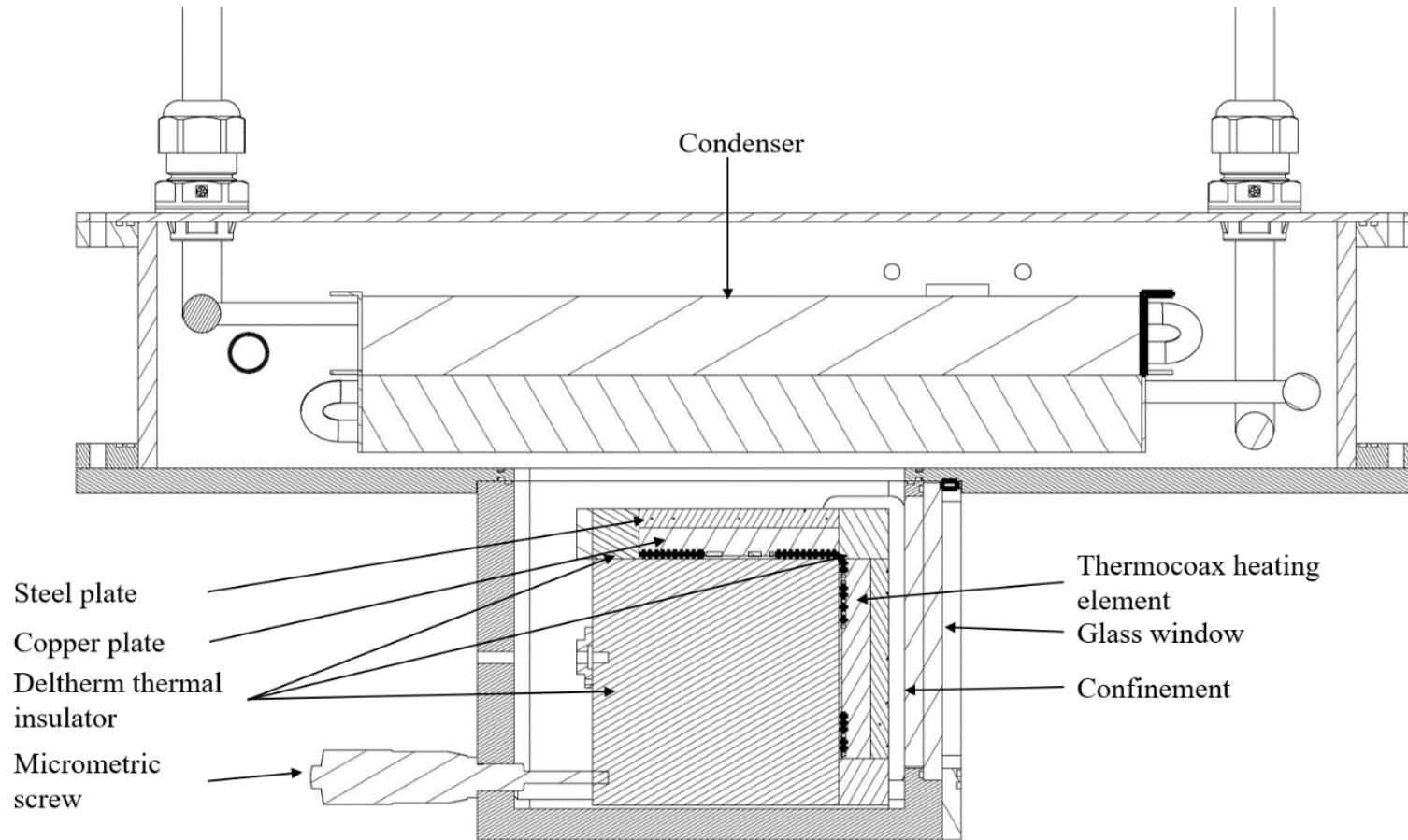
Heating elements

Two heated plates at a 90° angle

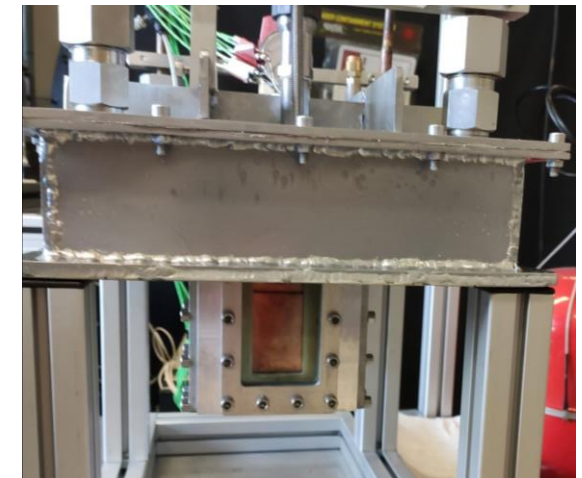


Experimental apparatus

General assembly



Side view



Front view

Experimental apparatus

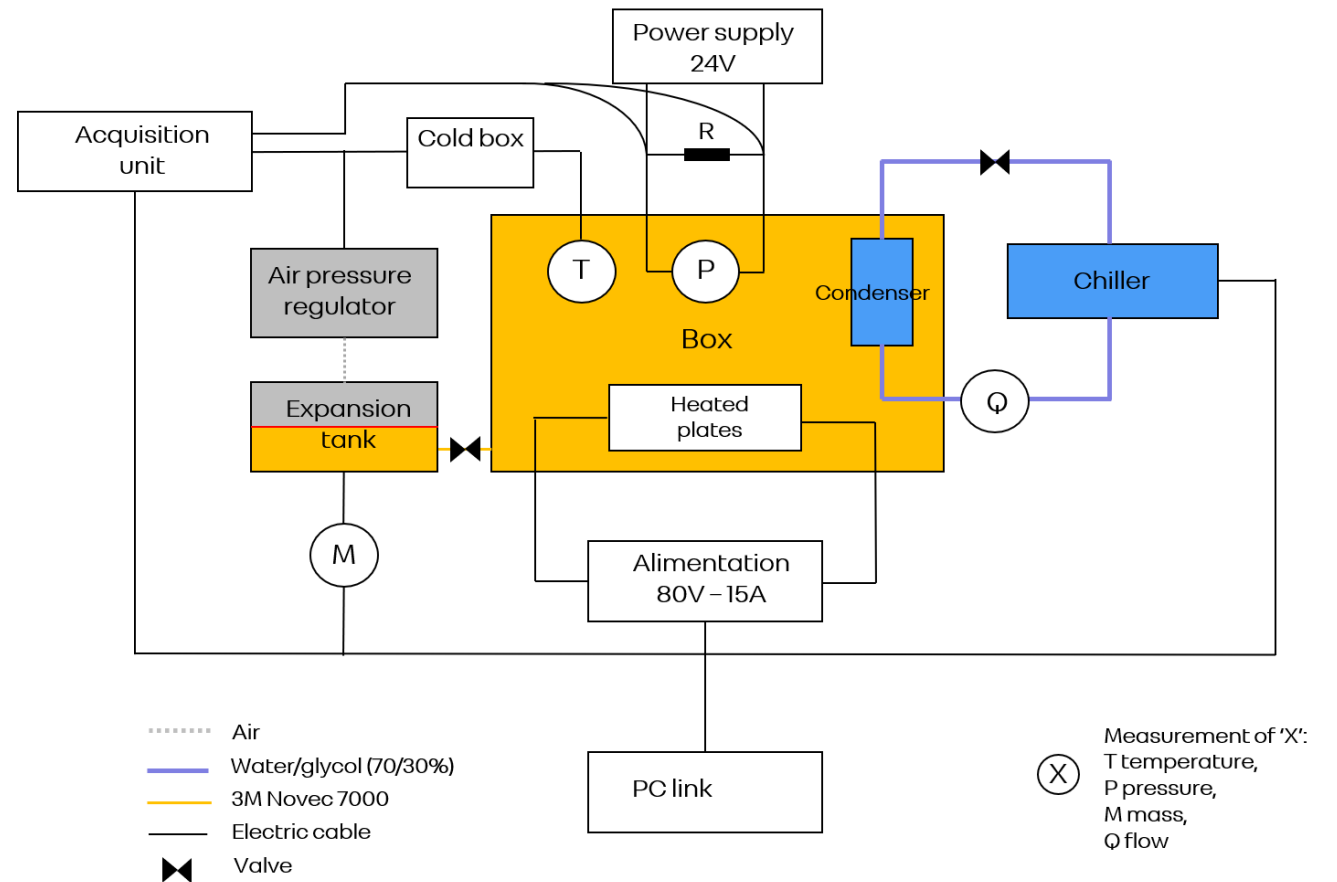
Measurements

45 K-type thermocouples in total:
-> in fluid and in heated plates

Absolute pressure sensor

Chiller to set condenser coolant mass flow and temperature

Expansion tank to regulate pressure



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Results and data analysis

Data reduction

Thermocouples at two depths to measure heat flux

$$T_S = T_1 - R_{th,1} q'' S \quad (1) \quad q'' S = \frac{T_2 - T_1}{R_{th,2}} \quad (2)$$

T_x : fluid temperature at x (°C)

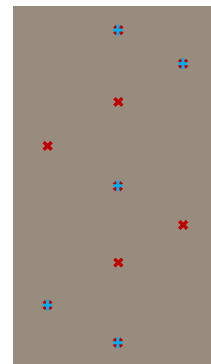
R_{th} : thermal conductive resistance (K/W)

q'' : heat flux density (W/m²)

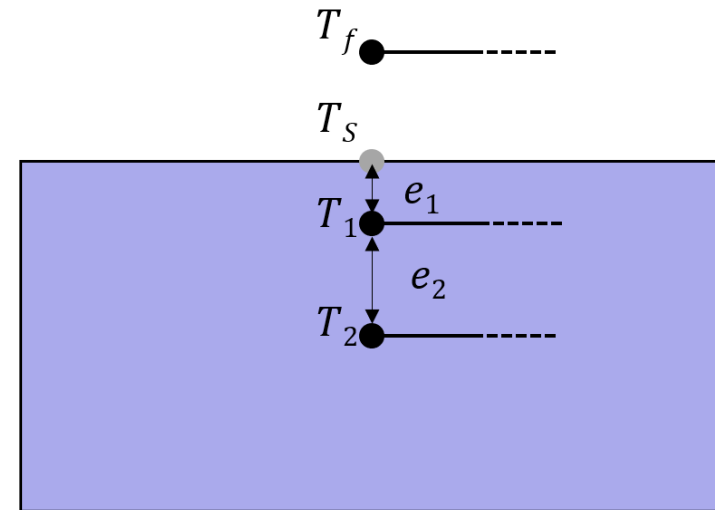
S : surface area perpendicular to heat flux (m²)

ΔT : wall superheat (°C)

h : heat exchange coefficient (W/m².K)



$e_1 = 0.7 \text{ mm}, e_2 = 2.3 \text{ mm}$



$$T_S = T_1 - \frac{e_1}{e_2} (T_2 - T_1) \quad (3)$$

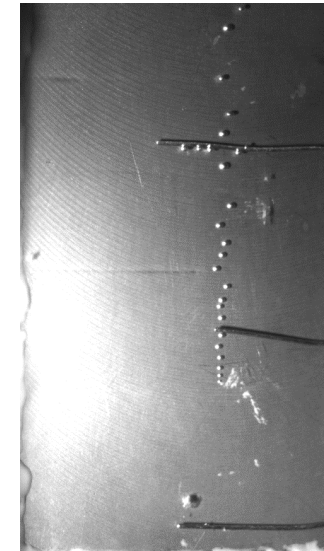
$$\Delta T = T_s - T_{sat}(P) \quad (4)$$

$$h = \frac{q''}{T_s - T_f} \quad (5)$$

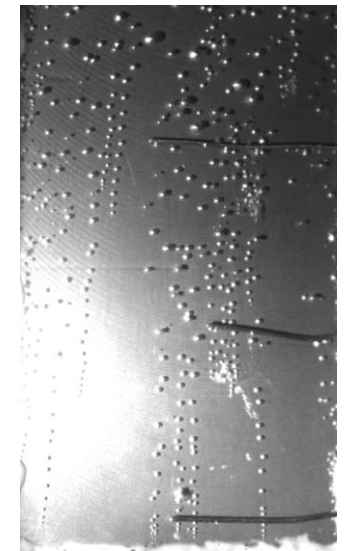
Results and data analysis

Experimental procedure

- Filling/draining/filtration of refrigerant
- Boiling hysteresis
- Testing procedure
- Repeatability test



Increasing heat flux



Decreasing heat flux

Boiling hysteresis
visualization at $0,3 \text{ W/cm}^2$

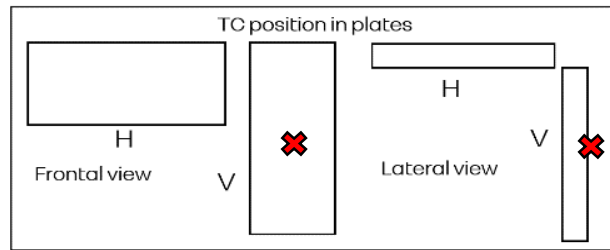
All boiling curves at decreasing heat flux

All points at atmospheric pressure (Novec 7000, $T_{\text{sat}} = 34^\circ\text{C}$)

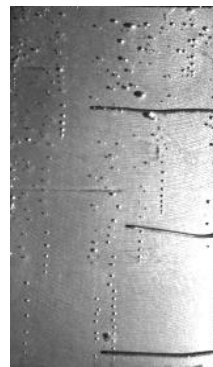
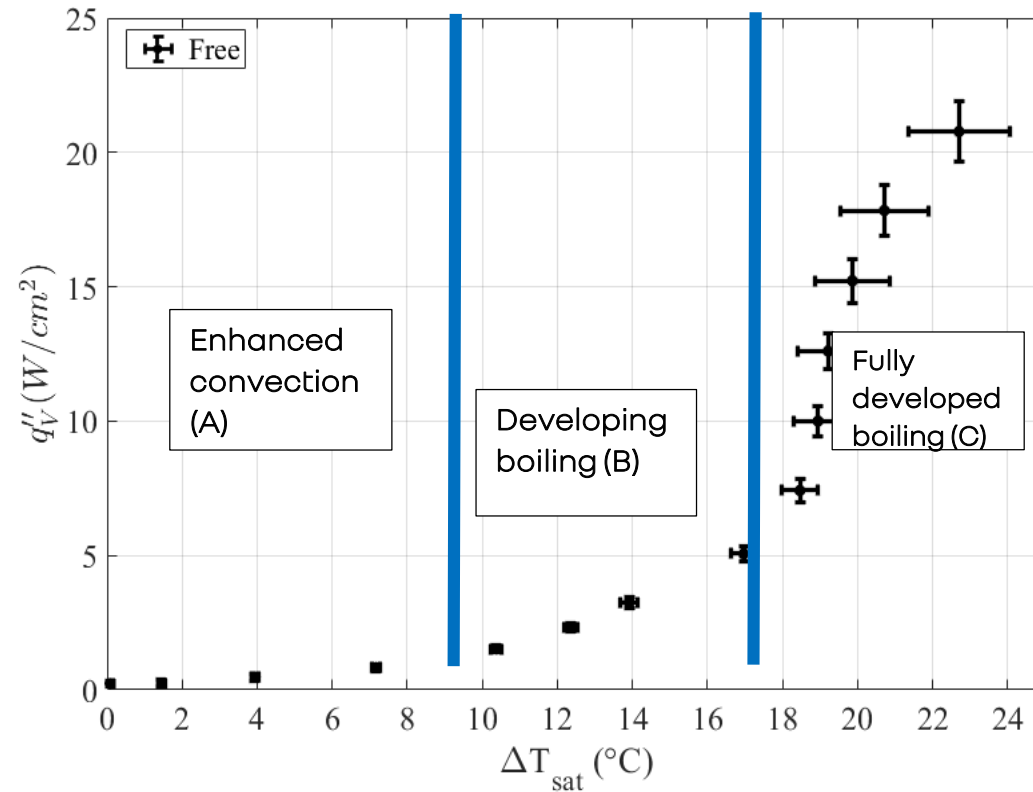
$e = [0.5; 15] \text{ mm} \Leftrightarrow \text{Bo} = [0.2; 245]$

Results & Data Analysis

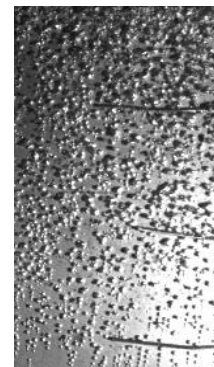
Free boiling curve



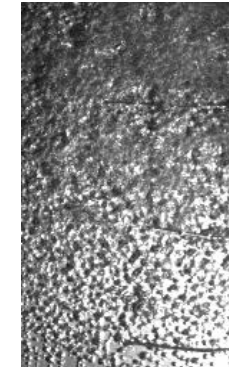
$T_{\text{condenser}} = 32\text{ }^{\circ}\text{C}$
Free configuration



(A)

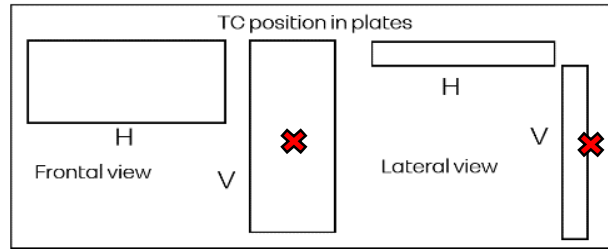


(B)

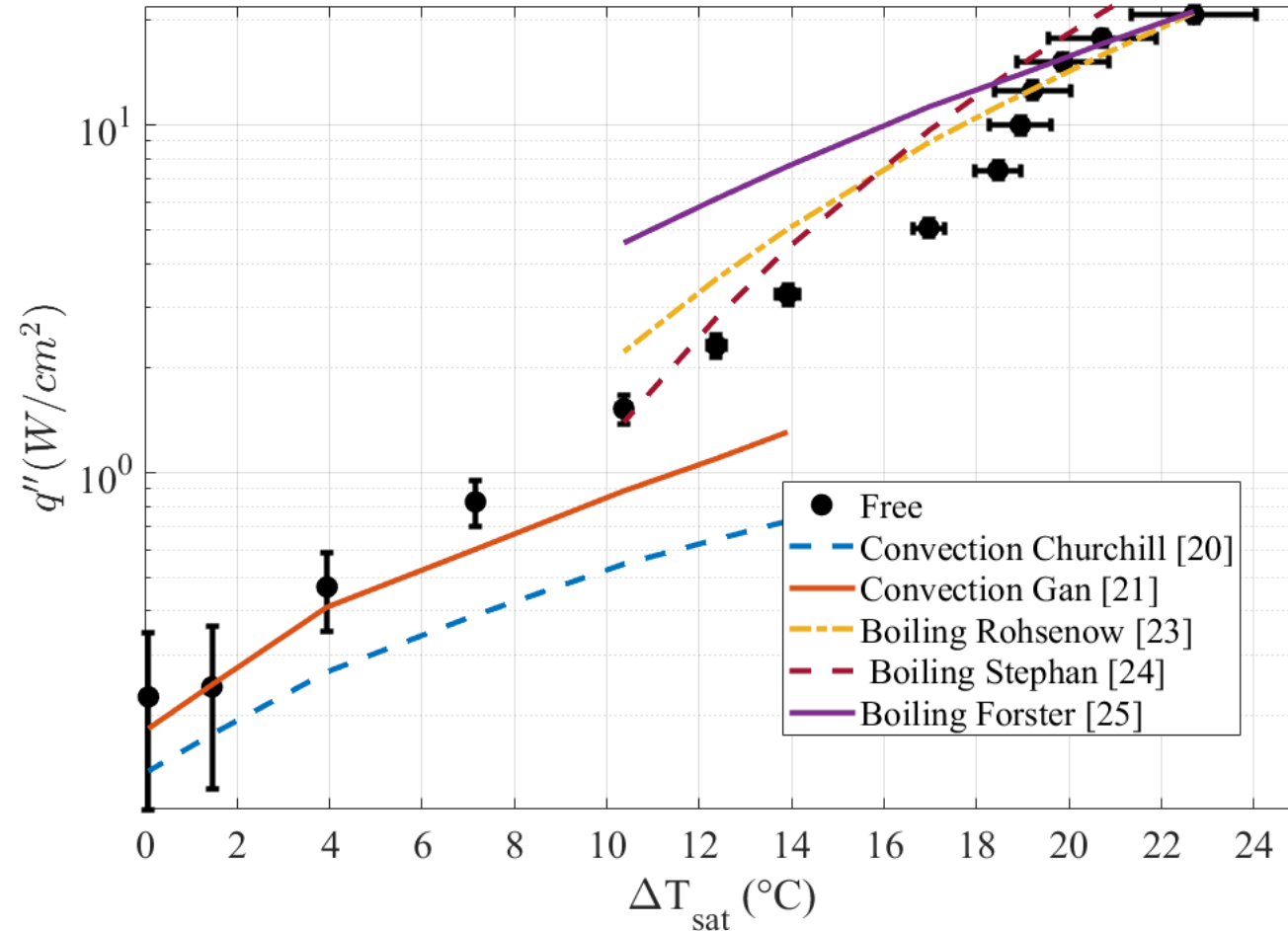


(C)

Free boiling curve

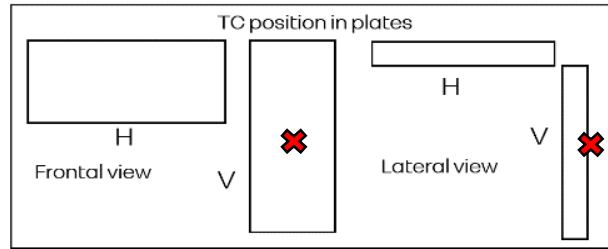


$T_{condenser} = 32^\circ\text{C}$
Free configuration



Experimental boiling curve against literature correlations

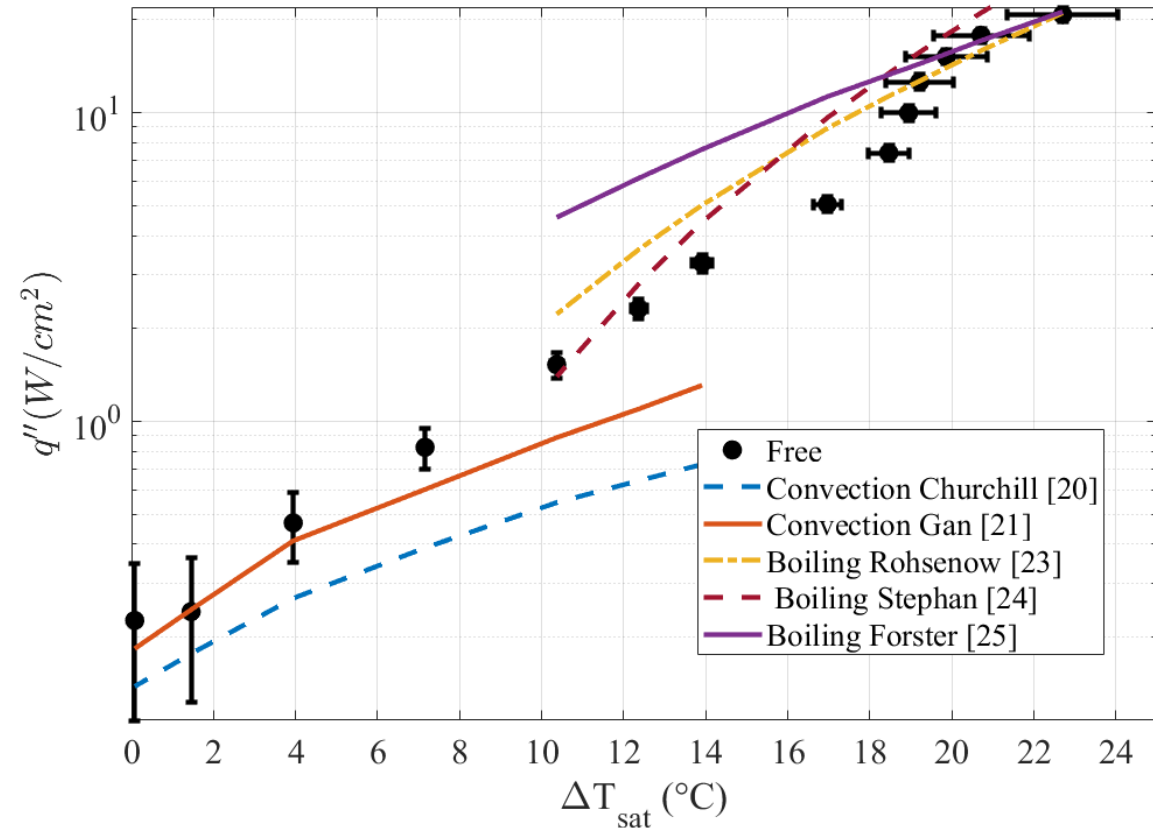
Free boiling curve



$T_{condenser} = 32^\circ\text{C}$
Free configuration

Perspectives :

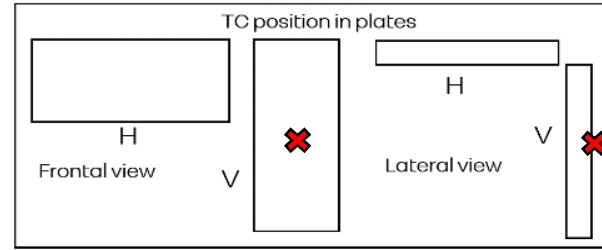
- Etude en convection naturelle
- Comparaison à ébullition en canal, prise en compte de x
- Etude sur toute la surface + paroi horizontale



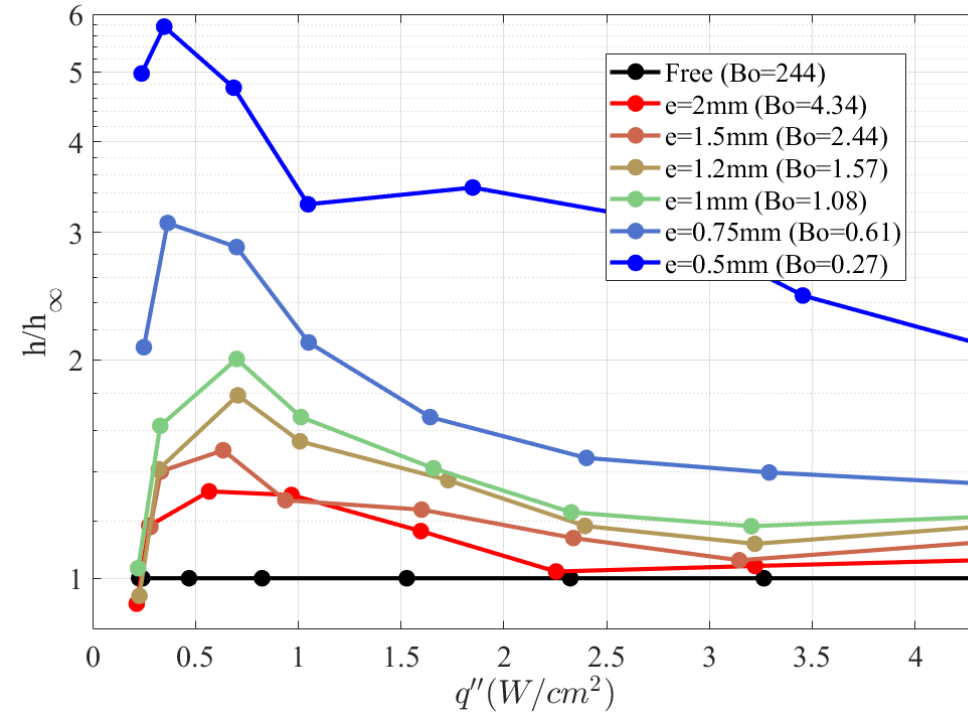
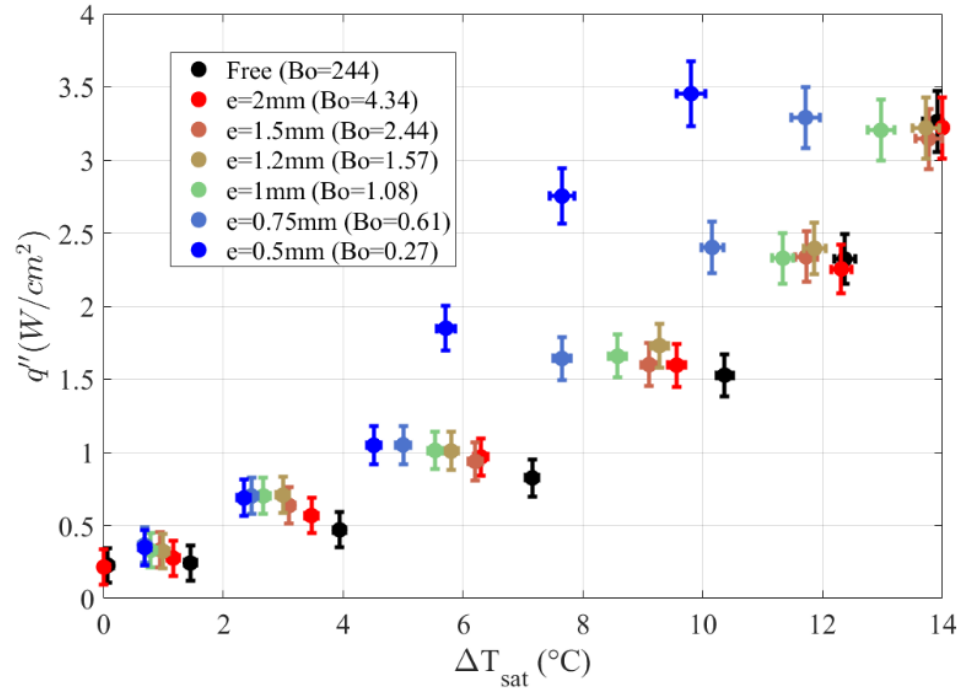
Experimental boiling curve against literature correlations

Résultats et analyse

Influence du confinement



$T_{\text{condenser}} = 32^\circ\text{C}$

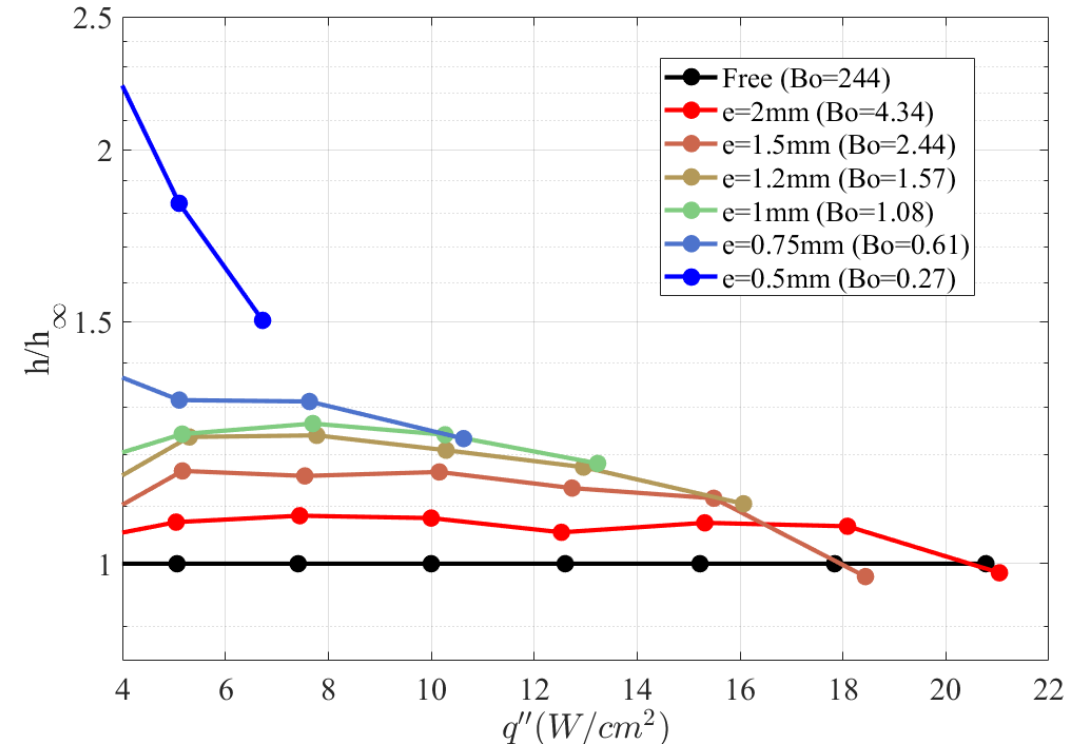
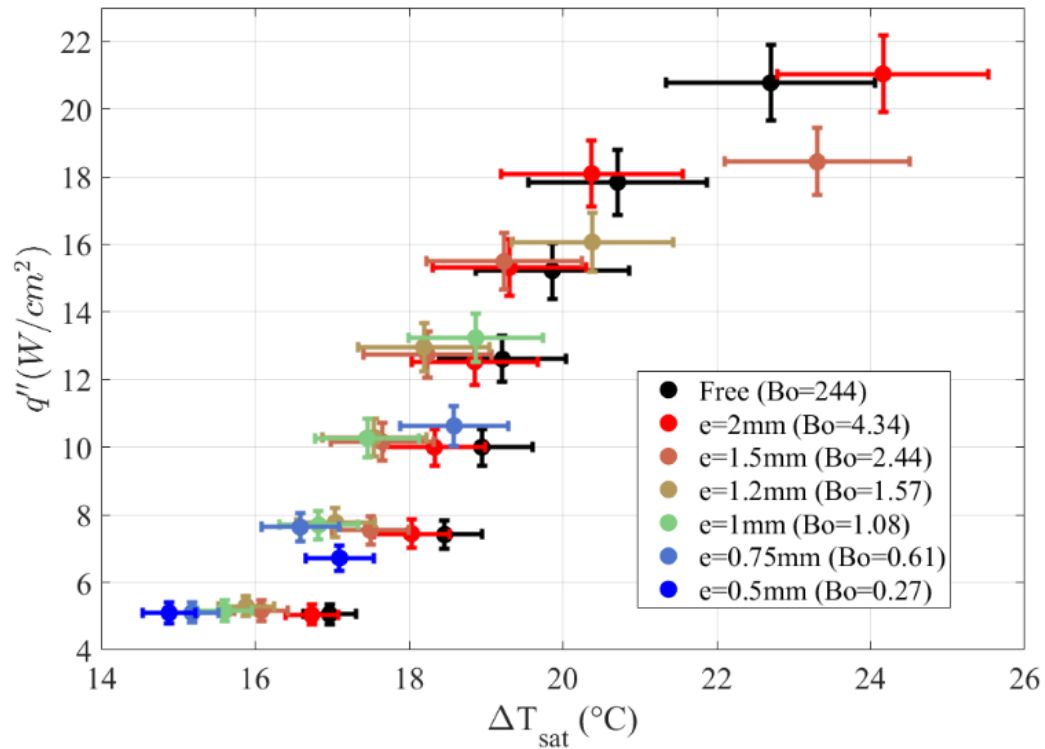


A bas flux:

- $e \nearrow \Delta T_{\text{sat}}$
- Influence de e sur ΔT_{sat} n'est pas linéaire
- HTC améliorés jusqu'à 600% à petit flux

Influence du confinement

$T_{\text{condenser}} = 32^\circ\text{C}$



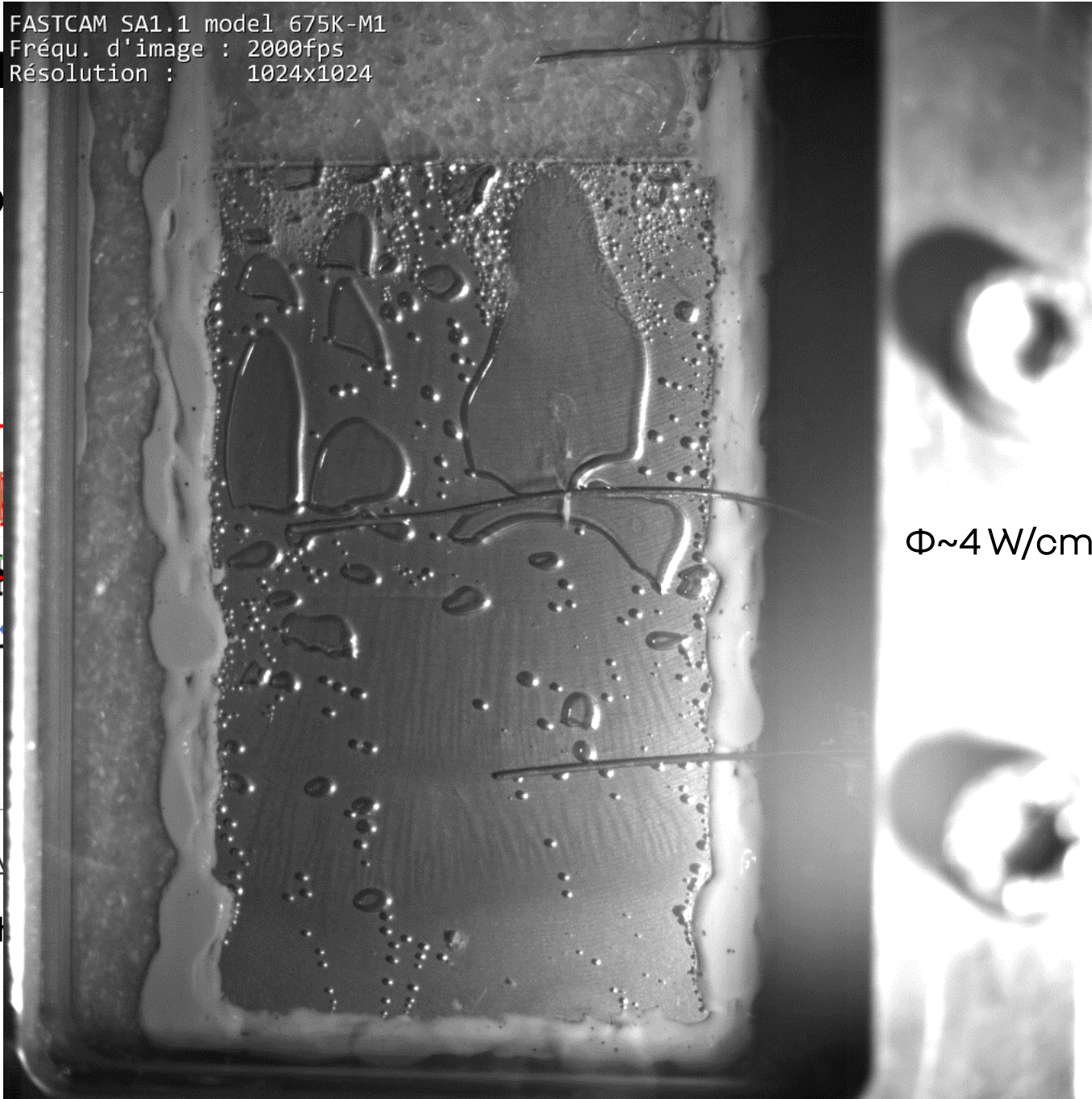
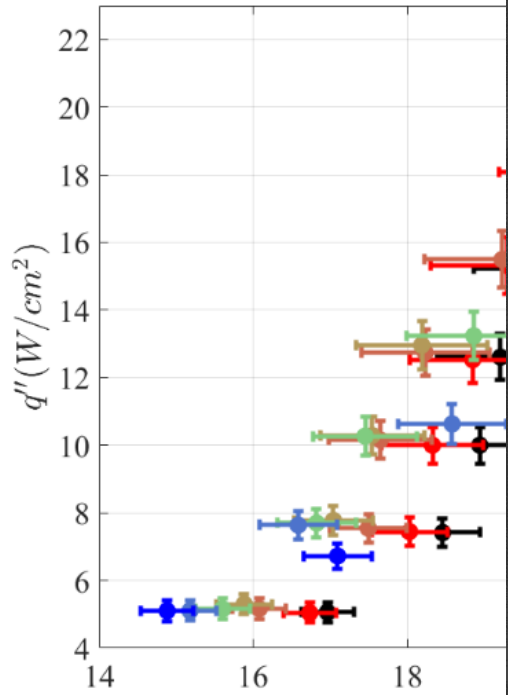
A haut flux:

- e a une influence négligéable (avant d'atteindre le flux critique)
- Configuration libre \approx épaisseurs de canal

Résultats et ana

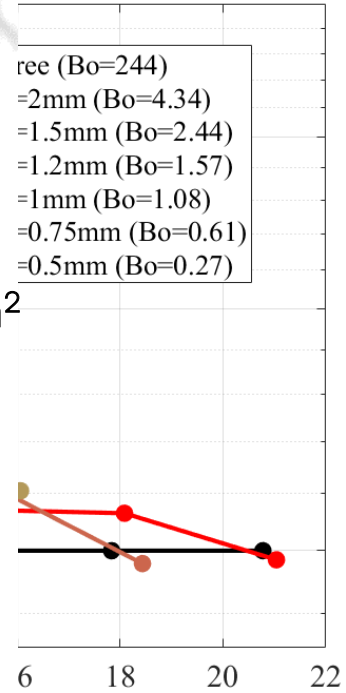
FASTCAM SA1.1 model 675K-M1
Fréq. d'image : 2000fps
Résolution : 1024x1024

Influence du co



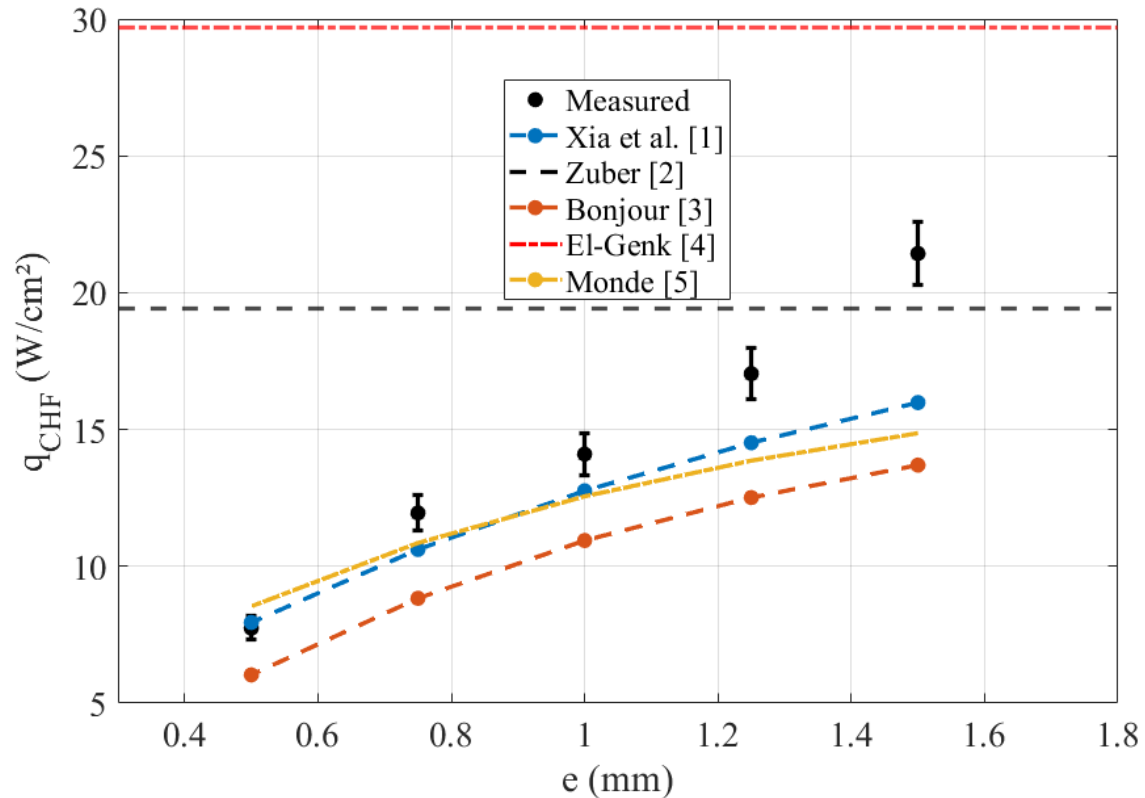
=32 °C

$\Phi \sim 4 \text{ W/cm}^2$



Δ
•
•

Critical heat flux

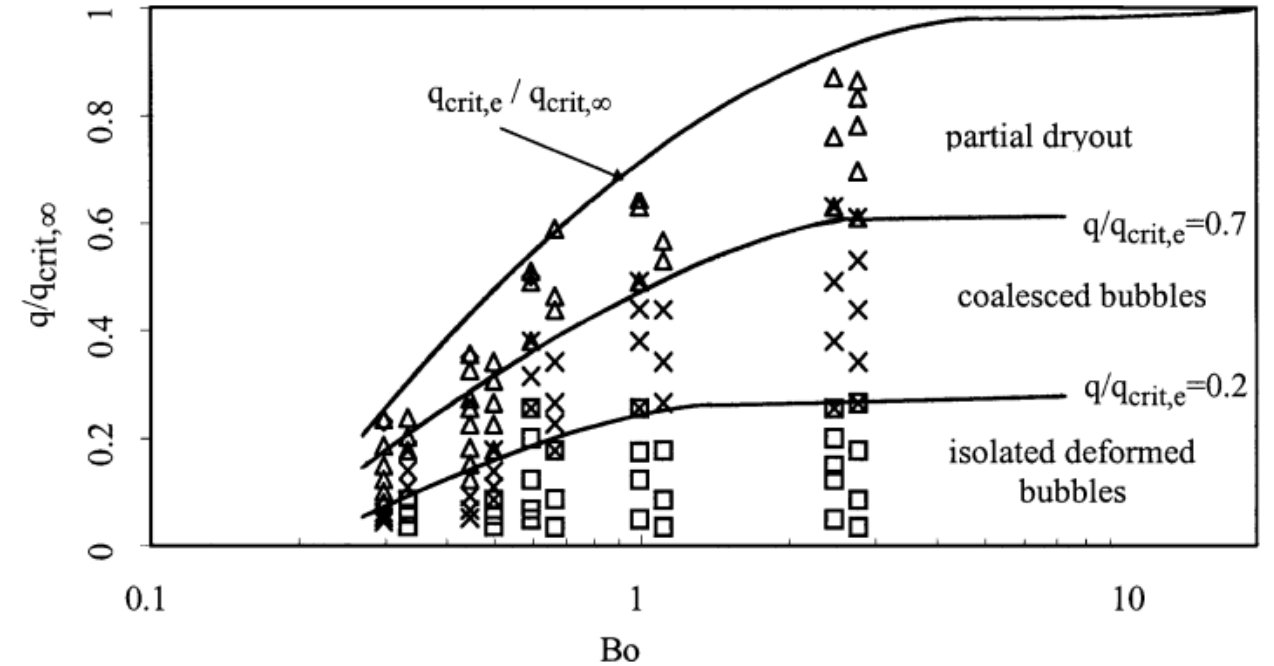
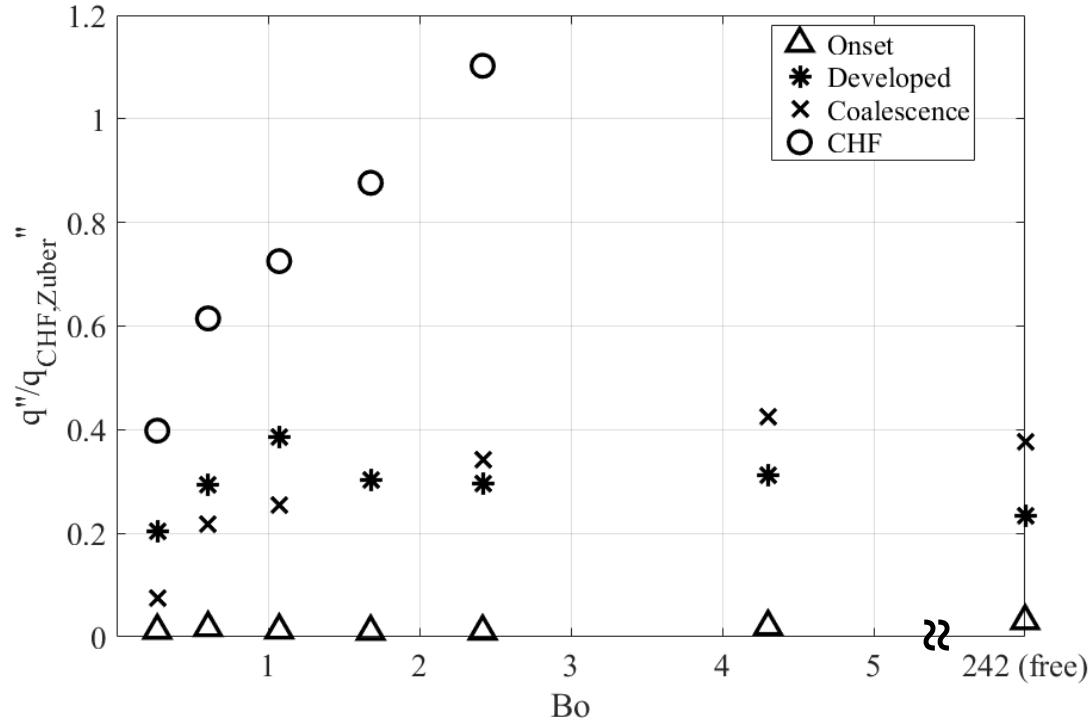


$$T_{\text{condenser}} = 32 \text{ }^{\circ}\text{C}$$

- CHF \searrow with e
- Zuber and El-Genk : not a function of e
- Xia et al: R-113 on vertical copper plate
- El-Genk : Novec 7000, $P=0,85$ bar and on copper vertical surface
- Bonjour: R-113 fluid on copper vertical surface
- Monde: R-113, benzene, water, ethanol with copper vertical heater

Difficulté à mesurer visuellement le début de l'assèchement partiel
 → Méthode retenue: changement pente des HTC

Patterns map



Bonjour et Lallemand, R-113 fluid, Int. J. Multiphase Flow 24 (1998)

- Same regime behaviour is confirmed
- Difficulty measuring start of partial dryout regime

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Present study conclusions

- Dedicated testbench for study Novec 7000 confined boiling
- Confinement ↗ heat exchange at low-medium heat flux (<10 W/cm²)
- Confinement ↗ heat exchange at high heat flux (>10 W/cm²)
- Confinement ↘ CHF
- 3 main boiling regimes observed

Perspectives for the future

Study of:

- subcooling
- onset of boiling
- surface rugosity
- pressure

Improve visual data treatment

Perspectives :

- Etude en convection naturelle
- Comparaison à ébullition en canal, prise en compte de x
- Etude sur toute la surface + paroi horizontale => manip plus fine
- Comparaison avec écoulement type Hel et Shaw
- Fluide non PFAS
- Transitoire

Remarques/Questions :

- Discussion autour des fluides de travail et de leur potentielle interdiction.
Certains ont de l'espoir dans des HFOs
- Quid de l'effet de la géométrie/effets de bord : Bonjour et al. => «cheminée»,
Lips et al. => caloduc plat mais pas forcément rempli entièrement, current
study => caloduc plat rempli mais espace sur les côtés

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Thank you!