

Ecoulements Compressibles Diphasiques avec Raffinement de Maillage Automatique

Two-fluid Compressible Flows with Multiresolution Adaptive Mesh Refinement

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Motivation

Crucial role of **boiling** in optimizing thermal performance in various industrial scenarios **Flows of interest**

Challenges of two-phase flow modelling \ast low Mach regime $M \ll 1$ (phase change, surface tension……)

Use **adaptive mesh refinement** strategy to improve efficiency and flexibility

- ✽ compressible gas + incompressible liquid
-

Objective: develop a **compressible** solver for liquid-gas flows

- \checkmark Accurate in interface capturing
- \checkmark Accurate in the low Mach regime
- \checkmark Capable of handling heat transfer and phase change
- \checkmark Integrated with an effective adaptive mesh refinement technique

Each phase is described by a compressible model

$$
\left\{ \begin{aligned} \partial_t \rho + \nabla \cdot (\rho \mathbf{u}) &= 0 \\ \partial_t (\rho \mathbf{u}) + \nabla \cdot (\rho \mathbf{u} \otimes \mathbf{u}) + \nabla p &= \nabla \cdot \mathbb{S} + \rho \boldsymbol{f} \\ \partial_t (\rho E) + \nabla \cdot ((\rho E + p) \mathbf{u}) &= \nabla \cdot (\mathbb{S} \mathbf{u}) + \rho \boldsymbol{f} \cdot \boldsymbol{u} + \nabla \cdot (\mathscr{K} \nabla T) \end{aligned} \right.
$$

$$
\begin{matrix} \vec{n} \\ \\ \\ \vec{D}_2 \end{matrix}
$$

ρ fluid density \boldsymbol{u} fluid velocity

 p fluid pressure viscous stress tensor

f volume forces E total energy

 $\mathcal K$ thermal conductivity

speed of sound

Equation of state

Ex: stiffened gas EOS, barotropic EOS

 \checkmark mass conservation \to **velocity jump**

$$
\llbracket \mathbf{u} \cdot \mathbf{n} \rrbracket_{\Gamma} = \dot{m}\llbracket \frac{1}{\rho} \rrbracket_{\Gamma}
$$

ü momentum balance → **pressure jump**

$$
\llbracket p \rrbracket_{\Gamma} = \sigma \kappa
$$

 \checkmark energy conservation \to **thermal flux jump**

$$
\llbracket \mathscr{K} \nabla T \rrbracket_{\Gamma} \cdot \mathbf{n} = \dot{m} L_\text{heat}
$$

 $\dot m$ phase change mass flow rate $L_{\rm heat}$ latent heat of vaporization $\mathbb{L} \cdot \mathbb{I}_\Gamma$

jump operator across the interface

Interface description: level set method

Level set advection

$$
\partial_t \phi + \mathbf{u}_\Gamma \cdot \nabla \phi = 0
$$

interface $\Gamma(t) = \{ \mathbf{x} \in \mathcal{D} \mid \phi(\mathbf{x},t) = 0 \}$

interface velocity \mathbf{u}_Γ

normal vec

normal vector
$$
\mathbf{n} = \frac{\nabla \phi}{|\nabla \phi|}
$$

interface curvature $\kappa = \nabla \cdot \left(\frac{\nabla \phi}{|\nabla \phi|}\right)$

Level set function

$$
\phi = \begin{cases} d(\mathbf{x},\Gamma) & \text{ for } \mathbf{x} \in \mathcal{D}_1, \\ 0 & \text{ for } \mathbf{x} \in \Gamma, \\ -d(\mathbf{x},\Gamma) & \text{ for } \mathbf{x} \in \mathcal{D}_2. \end{cases}
$$

Discretization 5th order One-Step scheme

[V. Daru et al., 2004, Zou et al., 2020]

 $|\nabla \phi|=1$ distance property

Reinitialization (redistancing)

 $\partial_\tau \phi = \text{sign}(\phi_0) (1-|\nabla \phi|)$

Finite Volume discretization

A single fluid Lagrange-Projection type scheme [C. Chalons et al., 2016]

Decomposition of the global system into 3 subsystems

6

Numerical discretization

Godunov approach

$$
L_j \rho_j^{n+} = \rho_j^n,
$$

\n
$$
L_j (\rho \mathbf{u})_j^{n+} = (\rho \mathbf{u})_j^n - \frac{\Delta t}{|\Omega_j|} \sum_{k \in \mathcal{N}(j)} |\partial \Omega_{jk}| \pi_{jk}^* \mathbf{n}_{jk} - \Delta t \{\rho \nabla \Psi\}_j,
$$

\n
$$
L_j (\rho E)_j^{n+} = (\rho E)_j^n - \frac{\Delta t}{|\Omega_j|} \sum_{k \in \mathcal{N}(j)} |\partial \Omega_{jk}| \pi_{jk}^* u_{jk}^* - \Delta t \{\mathbf{u}^* \rho \nabla \Psi\}_j,
$$

\n
$$
\phi_j^{n+} = \phi_j^n,
$$

\n
$$
L_j = 1 + \frac{\Delta t}{|\Omega_j|} \left(\sum_{k \in \mathcal{N}(j)} |\partial \Omega_{jk}| u_{jk}^* \right).
$$

 π surrogate pressure from Suliciu-type relaxation

Step 1. Acoustic step

 $n+$

[C. Chalons et al., 2016]

Approximate Riemann solver

Numerical flux for bulk cells

$$
u_{jk}^* = \frac{\mathbf{n}_{jk} \cdot (a_j \mathbf{u}_j + a_k \mathbf{u}_k)}{a_j + a_k} - \frac{\pi_k - \pi_j}{(a_j + a_k)}
$$

$$
\pi_{jk}^* = \frac{a_k \pi_j + a_j \pi_k}{a_j + a_k} + \frac{a_j a_k}{a_j + a_k} \mathbf{n}_{jk} \cdot (\mathbf{u}_j - \mathbf{u}_k)
$$

for interface cells (+ jump conditions)

$$
u_{jk}^* = \frac{\mathbf{n}_{jk} \cdot \left(a_j \mathbf{u}_j + a_k \mathbf{u}_k + a_k \widetilde{\lbrack\!\lbrack\mathbf{u}\rbrack\!\rbrack_{\Gamma_{jk}}}\rbrack}{a_j + a_k} + \frac{\pi_j - \pi_k - \widetilde{\lbrack\!\lbrack\mathbf{p}\rbrack\!\rbrack_{\Gamma_{jk}}}\rbrack}{a_j + a_k} \\ \pi_{jk}^* = \frac{a_k \pi_j + a_j \pi_k + a_j \widetilde{\lbrack\!\lbrack\mathbf{p}\rbrack\!\rbrack_{\Gamma_{jk}}}\rbrack}{a_j + a_k} + \frac{a_j a_k}{a_j + a_k} \mathbf{n}_{jk} \cdot (\mathbf{u}_j - \mathbf{u}_k - \widetilde{\lbrack\!\lbrack\mathbf{u}\rbrack\!\rbrack_{\Gamma_{jk}}}\rbrack}{\tau_j - \tau_k}
$$

$$
a_j=1.1\rho_j c_j, a_k=1.1\rho_k c_k \qquad \qquad \textbf{7}
$$

Low Mach analysis

$\tilde{\nabla} \tilde{p} = {\cal O}(M^2)$ **Low Mach regime**

Truncation errors of the dimensionless acoustic subsystem in the low Mach regime

Low Mach correction [Z. Zou et al., 2022]

$$
\partial_{\tilde t} \tilde \rho + \tilde \nabla \cdot \tilde {\bf u} = {\cal O}(\Delta \tilde t) + {\cal O}(M \Delta \tilde x),\\ \partial_{\tilde t} (\tilde \rho \tilde {\bf u}) + \tilde \rho \tilde {\bf u} \tilde \nabla \cdot \tilde {\bf u} + \frac{1}{M^2} \tilde \nabla \tilde p = {\cal O}(\Delta \tilde t) + {\cal O}(\frac{\Delta \tilde x}{M}),\\ \partial_{\tilde t} (\tilde \rho \tilde E) + \tilde \rho \tilde E \tilde \nabla \cdot \tilde {\bf u} + \tilde \nabla \cdot (\tilde p \tilde {\bf u}) = {\cal O}(\Delta \tilde t) + {\cal O}(M \Delta \tilde x).
$$

Dimensionless variables

$$
\tilde{\rho}=\rho/\hat{\rho}_i,\quad \tilde{p}=p/\hat{p}_i,\quad \tilde{c}=c/\hat{c}_i,\quad \tilde{e}=e/\hat{e}_i,\quad i=1,2
$$

Asymptotic expansion

$$
p(t,\mathbf{x})=M^0p^{(0)}(t,\mathbf{x})+M^1p^{(1)}(t,\mathbf{x})+M^2p^{(2)}(t,\mathbf{x})+\cdots
$$

$$
\begin{aligned} &\left(u_{jk}^{*,\theta}=(1-\theta_{jk})\Bigg(\mathbf{n}_{jk}\cdot\frac{\mathbf{u}_j+\mathbf{u}_k+\llbracket\mathbf{u}\rrbracket_{\Gamma_{jk}}}{2}+\frac{\pi_j-\pi_k-\llbracket p\rrbracket_{\Gamma_{jk}}}{a_j+a_k}\Bigg)+\theta_{jk}u_{jk}^*\\ &\pi_{jk}^{*,\theta}=(1-\theta_{jk})\frac{\rho_k\pi_j+\rho_j\Big(\pi_k+\llbracket p\rrbracket_{\Gamma_{jk}}\Big)}{\rho_j+\rho_k}+\theta_{jk}\pi_{jk}^*\\ &\left(\theta_{jk}=\min\bigg(\frac{u_{jk}^*}{\max(c_j,c_k)},1\bigg)\right)\end{aligned}
$$

uniform truncation error with respect to Mach number **Step 2. Transport step**

Upwind scheme + ghost fluid method (linear extrapolation)

$$
\partial_t b + \nabla \cdot (b \mathbf{u}) + b \nabla \cdot \mathbf{u} = 0 \qquad b = (\rho, \rho u, \rho v, \rho E)^\mathbf{T}
$$

$$
b_j^{n+1-} = b_j^{n+} - \frac{\Delta t}{|\Omega_j|} \sum_{k \in \mathcal{N}(j)} |\partial \Omega_{jk}| u_{jk}^* \overline{b_{jk}^{n+1}} + b_j^{n+} \frac{\Delta t}{|\Omega_j|} \sum_{k \in \mathcal{N}(j)} |\partial \Omega_{jk}| u_{jk}^*
$$

$$
b_{jk}^{n+} = \begin{cases} b_j^{n+} & \text{if } u_{jk}^* > 0, \\ b_k^{n+} & \text{if } u_{jk}^* \le 0 \text{ and } \phi_j \phi_k > 0, \\ b_{k,ghost}^{n+} & \text{if } u_{jk}^* \le 0 \text{ and } \phi_j \phi_k < 0. \end{cases}
$$

Step 3. Diffusion step

Discretization of **viscous diffusion** Centered second-order FV method

Discretization of **heat diffusion** near the interface

Without phase change, continuous heat flux across the interface $\mathscr{K}_j \frac{T_j - T_{\Gamma_j}}{\Delta x_i^{\Gamma}} = \mathscr{K}_k \frac{T_{\Gamma_j} - T_k}{\Delta x_k^{\Gamma}}$

1

interface temperature **interface** interface interface

$$
T_{\Gamma_j}=\frac{\mathscr{K}_jT_j\Delta x_k^{\Gamma}+\mathscr{K}_kT_k\Delta x_j^{\Gamma}}{\mathscr{K}_j\Delta x_k^{\Gamma}+\mathscr{K}_k\Delta x_j^{\Gamma}}
$$

$$
\mathscr{K}_{j}\nabla T_{\Gamma_{j}}\cdot\mathbf{n}_{jk}=\mathscr{K}_{j}\frac{T_{\Gamma_{j}}-T_{j}}{\Delta x_{j}^{\Gamma}}
$$

With phase change, discontinuous heat flux **2**

assumption $T_{\Gamma} = T_{\text{sat}}$

Compute phase change mass flow rate from heat flux

[Y. Sato et al., 2013, S. Tanguy et al., 2014]

$$
\llbracket\mathscr{K}\nabla T\rrbracket_{\Gamma}\cdot\mathbf{n}=\dot{m}L_{\text{heat}} \qquad \qquad \Longleftrightarrow \qquad \left|\begin{array}{c} \dot{m}=\frac{-k_{\text{liq}}\nabla T_{\text{liq}}\cdot\mathbf{n}+k_{\text{vap}}\nabla T_{\text{vap}}\cdot\mathbf{n}}{L_{\text{heat}}}\cr \cr \cr \cr \cr \end{array}\right.
$$

Compute interface velocity for $\partial_t \phi + \boxed{\mathbf{u}_\Gamma} \cdot \nabla \phi = 0$

$$
\llbracket \mathbf{u}\cdot \mathbf{n}\rrbracket_{\Gamma} = \dot{m}\llbracket \frac{1}{\rho}\rrbracket_{\Gamma} \qquad \qquad \overbrace{\qquad \qquad } \qquad \overbrace{\qquad \qquad } \qquad \overbrace{\qquad \qquad } \qquad \overbrace{\qquad \qquad } \qquad \qquad } \overbrace{\qquad \qquad } \overbrace{\qquad \qquad } \qquad \qquad } \overbrace{\qquad \qquad } \overbrace{\
$$

Compute heat flux at the interface

Depends on how to approximate the temperature gradient

use neighboring cell belonging to the **same fluid**

[Y. Sato et al., 2013, L. Anumolu et al., 2018]

Linear sloshing

 $\mathbf{g}% _{T}=\mathbf{g}_{T}=\math$

 \uparrow

 ${\cal L}$

 $|a_0/$

 $h_{\rm gas}$

 h_{liquid}

spatial resolution: 32 * 72

Rayleigh-Taylor instabilities

 $Ma < 10^{-3}$

interface initial position:

 $y=1-0.15\sin(2\pi x)$

1D non-isothermal problem

Reference: ALE, incompressible liquid + compressible gas

Stefan problem $Ja=2$

$$
Ja = \frac{\rho_l C_{p,l} (T_{\max} - T_{\mathrm{sat}})}{\rho_v L_{\mathrm{heat}}}
$$

Temporal evolution of interface position x_{Γ}

 $\rho_{\mathrm{liquid}}/\rho_{\mathrm{vapor}} = 10$

Stefan problem $Ja=30$

$$
\rho_{\rm liquid}/\rho_{\rm vapor}=1600
$$

 $L/\Delta x = 65$

Temporal evolution of the liquid velocity.

Mesh refinement strategy

Aim: improve computational efficiency and flexibility

Adaptive Mesh Refinement (AMR) Network and Multi-Resolution Analysis (MRA)

Based on empirical, a posteriori criteria (gradient, local residuals……)

Implementation

Based on a rigorous mathematical analysis of wavelet theory.

Use a local wavelet basis whose coefficients provide an accurate measure of the local regularity. Adapt the mesh according to its local regularity.

 \checkmark C++

- \checkmark Able to handle both AMR and MRA
- \checkmark @CMAP, École Polytechnique

https://github.com/hpc-maths/samurai

Multi-resolution example: discretization by point values

Multi-resolution example: 1D function

Multiresolution on 1D function [C. Tenaud et al., 2011]

Uniform mesh (grid level 5, 32 grid points) and **MR mesh** (four grid levels [2, 5])

MR mesh for Stefan problem

mesh compression rate = 79.4%

Local grid refinement

threshold parameter on each grid level l :

$$
\varepsilon_l = 2^{N_{\mathrm{dim}}\cdot (l-L)} \varepsilon
$$

 N_{dim} dimension

- L the finest grid level
- ϵ tolerance specified by user

scaled by global maximum :

Remark:

- value of $\epsilon, 0 < \epsilon \ll 1$ has a leading role in the accuracy and efficiency
- *details* decay with the grid level for smooth solutions, and recover large values in discontinuous regions

[C. Tenaud et al., 2015]

Rayleigh-Taylor instabilities + MR

In practice:

Compromise between accuracy and compression rate MR mesh $\varepsilon = 0.01, r = 2$

 $t^* = 2.35$ **24**

Summary and Outlook

Objective: \odot

- \checkmark Accurate in interface capturing
- \checkmark Accurate in the low Mach regime
- \checkmark Capable of handling heat transfer and phase change
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A two-fluid compressible solver

- \triangleright interface is captured by level set method
- \triangleright with low Mach correction
- \triangleright with sharp-interface phase change model
- \triangleright with multiresolution adaptive mesh refinement

Work in progress

- \triangleright Evaluate the performance of multiresolution (error analysis, computational time, mesh compression)
- \triangleright Extend to 2D bubble boiling case

Thank you for your attention! Questions?

Rayleigh-Taylor instabilities + MR

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